



Crude Preheat Curramix Coating Study

Objectives:

This study evaluates a Crude preheat exchanger service heat transfer performance with the following tube material and coatings and estimates the energy savings and CO2 Emissions Reduction:

- Carbon Steel
- Stainless Steel
- Carbon Steel Tube ID Coated
- Stainless Steel Tube ID Coated

Assumptions

- Service Desalted Crude vs Heavy Vacuum Gas Oil (HVGO)
- Tube ID Coating Thickness 25 Microns (0.001 inch)
- Coating Thermal Conductivity 0.722 Btu/hr-ft-F
- Fuel Value -\$3.50 per MBtu/hr
- Furnace Efficiency = 0.9
- Network Factor = 0.75 [Part of the Duty Gain in the Exchanger Diminishes Heat Transfer on other Exchangers in the Preheat Train due to changes in temperature differentials]
- CO2 Reduction based on EPA Conversion Equations
- Heat Transfer Calculation performed with HTRI XIST
- Assumed Fouling Factor shown in the Comparison Tables below



• Assumed Inlet Operating

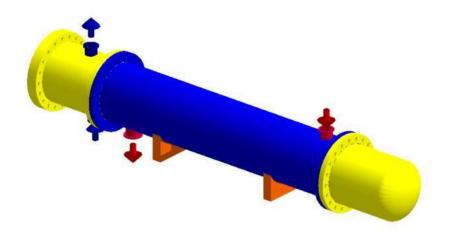
- \circ Crude Inlet Temp 370 F
- Crude Rate 650 klb/hr
- HVGO Inlet Temp 505 F
- HVGO Rate 675 klb/hr
 - Stream Properties

Hot Shellside Fluid		Inlet	Outlet	
Fluid name		VHGO		
Flow	(1000-lb/hr)	675.	00	
Temperature	(F)	505.00	475.18	
Pressure	(psia)	111.67	107.09	
Weight fraction vapor	()	0.0000	0.0000	
Vapor Prope	rties			
Flow	(1000-lb/hr)	-		
Density	(lb/ft3)		1.97	
Viscosity	(cP)	-	5.55	
Conductivity	(Btu/hr-ft-F)			
Heat capacity	(Btu/lb-F)			
Molecular weight	()			
Liquid Prope	rties			
Flow	(1000-lb/hr)	675.00	675.00	
Density	(lb/ft3)	46.741	47.559	
Viscosity	(cP)	1.4807	1.5337	
Conductivity	(Btu/hr-ft-F)	0.0528	0.0537	
Heat capacity	(Btu/lb-F)	0.6831	0.6657	
Molecular weight	()	-		
Latent heat	(Btu/lb)		1.55	
Surface tension	(dyne/cm)	0.0000	0.0000	

Cold Tubeside Fluid		Inlet	Outlet	
Fluid name		Crude		
Flow	(1000-lb/hr)	650.	00	
Temperature	(F)	370.00	402.61	
Pressure	(psia)	381.37	372.57	
Weight fraction vapor	()	0.0000	0.0000	
Vapor Prope	rties			
Flow	(1000-lb/hr)			
Density	(lb/ft3)	1.77	-	
Viscosity	(cP)	075		
Conductivity	(Btu/hr-ft-F)			
Heat capacity	(Btu/lb-F)		-	
Molecular weight	()	-	1	
Liquid Prope	rties			
Flow	(1000-lb/hr)	650.00	650.00	
Density	(lb/ft3)	44.085	42.918	
Viscosity	(cP)	0.8648	0.6984	
Conductivity	(Btu/hr-ft-F)	0.0671	0.0646	
Heat capacity	(Btu/lb-F)	0.6233	0.6342	
Molecular weight	()			
Latent heat	(Btu/lb)	-		
Surface tension	(dyne/cm)	0.0000	0.0000	



- Heat Exchanger Geometry
 - TEMA-AES
 - Shell Id = 50"
 - 1054 Tubes
 - 1" Tube OD
 - 0.083" tube wall thickness
 - 4 Tube Passes
 - 20 ft length
 - 11 Baffle Cross Passes, Single Vert Seg , 20.9% Cut

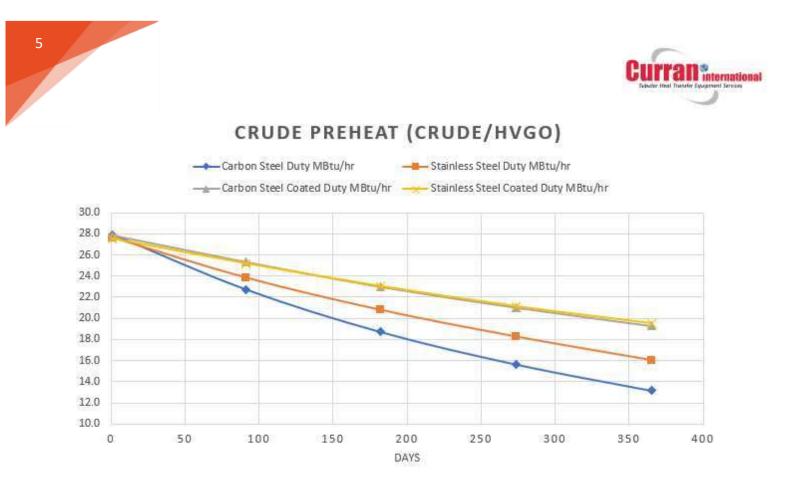




Results

Comparison Tables

111	i dilimenti i	242.4	Contraction and the	Carbon	Steel	and the second sec
Days	Qactual	Qclean	Qact/Qclean	Tubeside DP	Tubeside Fouling Factor	Shellside Fouling Factor
	MBtu/hr	MBtu/hr		psi	ft2-hr-F/Btu	ft2-hr-F/Btu
1	27.9	27.9	1.00	3.9	0.0000	0.0000
91	22.7	27.9	0.81	4.7	0.0044	0.0013
182	18.7	27.9	0.67	5.8	0.0088	0.0025
274	15.6	27.9	0.56	7.1	0.0131	0.0038
365	13.2	27.9	0.47	8.8	0.0175	0.0050
				Stainles	s Steel	
Days	Qactual	Qclean	Qact/Qclean	Tubeside DP	Tubeside Fouling Factor	Shellside Fouling Factor
100	MBtu/hr	MBtu/hr		psi	ft2-hr-F/Btu	ft2-hr-F/Btu
1	27.6	27.6	1.00	3.9	0.0000	0.0000
91	23.8	27.6	0.86	4.5	0.0030	0.0010
182	20.8	27.6	0.75	5.1	0.0060	0.0020
274	18.2	27.6	0.66	5.1	0.0090	0.0030
365	16.0	27.6	0.58	6.7	0.0120	0.0040
Days	Qactual	Qclean	Ca Qact/Qclean	rbon Steel Coa Tubeside DP	ted (0.001 inch) Tubeside Fouling Factor	Shellside Fouling Factor
-						
2012	MBtu/hr	MBtu/hr		psi	ft2-hr-F/Btu	ft2-hr-F/Btu
1	27.8	27.8	1.00	3.9	0.0000	0.0000
91	25.3	27.8	0.91	4.2	0.0015	0.0013
182	23.0	27.8	0.83	4.5	0.0030	0.0025
274	21.0	27.8	0.75	4.8	0.0045	0.0038
365	19.3	27.8	0.69	5.1	0.0060	0.0050
			Sta	inless Steel Coa	ated (0.001 inch)	
Days	Qactual	Qclean	Qact/Qclean	Tubeside DP	Tubeside Fouling Factor	Shellside Fouling Factor
	MBtu/hr	MBtu/hr		psi	ft2-hr-F/Btu	ft2-hr-F/Btu
1	27.5	27.5	1.00	3.9	0.0000	0.0000
91	25.2	27.5	0.91	4.2	0.0015	0.0010
182	23.0	27.5	0.84	4.5	0.0030	0.0020
274	21.1	27.5	0.77	4.8	0.0045	0.0030
365	19.5	27.5	0.71	5.1	0.0060	0.0040



Economic & CO2 Reduction Benefit

- 1. Coated Versus Carbon Steel
 - Annualized Duty Reduction = 3.6 MBtu/hr
 - Energy benefit = \$93k a year
 - CO2 Equivalent Benefit = 1,407 Tons a year
- 2. Coated Versus Stainless Steel
 - Annualized Duty Reduction = 2.0 MBtu/hr
 - Energy benefit = \$50k a year
 - CO2 Equivalent Benefit = 760 Tons a year

Note if the Crude preheat furnace is limited and/or the Preheat Train is Hydraulicly limited, the margin benefits could be significant more than the credits listed above.